

MATERIAL BALANCE

Basis: 100 Kg moles of C_2H_4O

The conversion is taken as 95%

Of the 100 Kg moles of ethylene oxide sent, 95% is reacting.

The crude stream 'a' contain the products and 5 Kg moles of C_2H_4O

Neglecting the 5 Kg moles of C_2H_4O i.e. assuming that all the 5 Kg moles of C_2H_4O are going out with the top product of the tower.

On a ethylene oxide free basis. The weight fraction (%) of crude product Stream 'a' is:

85% - Monoglycol ether

10% - Diglycol ether

5% - Triglycol ether

The mole fraction of this stream 'a' on a ethylene oxide free basis is as:

89.885% - Monoglycol ether

7.101% - Diglycol ether

3.011% - Triglycol ether

For a crude product of 100 Kg moles (C_2H_4O -free),

89.885 Kg moles of monoglycol ether => 89.885 Kg moles of C_2H_4O

7.101 Kg moles of carbitol => 14.202 Kg moles of C_2H_4O

3.011 Kg moles of triglycol ether => 9.033 Kg moles of C_2H_4O

Therefore, Total ethylene oxide that has reacted for 100 Kg moles of (C_2H_4O -free) crude product = 113.12 Kg moles of C_2H_4O .

For 100 Kg moles of C_2H_4O sent only 95 Kg moles reacts.

Therefore, for 95 Kg moles of C_2H_4O reacting, the total crude product (C_2H_4O -free) formed is

$(95 \times 100)/113.12 = 83.981$ Kg moles of crude product

The crude product is $(83.981+5)$ Kg moles for 100 Kg moles of C_2H_4O feed.

The total C_2H_5OH reacting = $[(83.981 \times 89.885)/100 + (83.981 \times 7.101)/100]$
= 81.4504 Kg moles

The recycle must be such that the ratio is 1:6

Total recycle is: $(6 \times 100) - 81.450 = 518.5$ Kg moles

The composition of the stream b is

518.55 Kg moles of $C_2H_4O + (83.981+5)$ Kg moles of crude product

The composition of stream 'a' on a C_2H_4O free basis is known.

For tower (1):

$$F = 83.981$$

$$F = D + W \text{-----(1)}$$

$$\text{And } Fx_F = Dx_D + Wx_W \text{-----(2)}$$

Now fixing x_D as 0.99 and $x_W = 0.05$, $x_F = 0.89885$

We have solving (1) and (2):

$$83.981 \times 0.89885 = D \times 0.99 + (83.981 - D) \times 0.05$$

Solving for D we have

$$D = 75.837 \text{ Kg moles}$$

$$\text{And } W = 8.143 \text{ Kg moles}$$

Let us take the 0.01 mole fraction lost in distillate is all carbitol (it is lighter than triglycol ether)

Therefore carbitol lost above is 0.75837 Kg moles

Now $W = 8.143$ Kg moles and has $(8.143 \times 0.05) = 0.40715$ Kg moles of mono-glycol ether

The carbitol in crude stream 'a' on a C_2H_4O free basis is

$$= (83.981 \times 7.101)/100$$

= 5.963 Kg moles

Of this 5.963 Kg moles of carbitol, 0.75837 Kg moles of carbitol is lost in distillate.

Therefore carbitol present = $5.963 - 0.75837$
= 5.205 Kg moles

The remaining in triglycol ether = $8.143 - 5.205 - 0.40715$
= 2.5307

For tower (2):

$F = 8.143$ Kg moles

Fixing x_D as 0.99 and this is the purity of the product and $x_W = 0.05$

We have $F = D + W$

$Fx_F = Dx_D + Wx_W$

And x_F of carbitol = $5.205/8.143 = 0.639$

$8.143 \times 0.6391 = D \times 0.99 + (8.143 - D) \times 0.05$

Solving for D we get

$D = 5.1040$ Kg moles

And $W = 3.038$ Kg moles

For 100 Kg moles of feed we have

5.1040 Kg moles of carbitol of 0.99 purity

25 TPD = 186.567 Kg moles/day

The ethylene oxide feed is 3655.309 Kg mole/day

The C_2H_5OH feed is $(81.450 \times 186.567) / 5.1040$
= 2977.249 Kg mole/day

Crude product (C_2H_4O -free) is $(83.981 \times 3655.309) / 100$

$$=3069.765 \text{ Kg mole/day}$$

Crude product with $\text{C}_2\text{H}_4\text{O}$ is $(88.981 \times 3655.309)/100$

$$= 3252.530 \text{ Kg moles/day}$$

The $\text{C}_2\text{H}_4\text{O}$ recycle is $(518.55 \times 3655.309)/100$

$$= 18954.558 \text{ Kg mole/day}$$

Mono glycol ether, distillate tower (1) $=75.837 \times 36.55309$

$$=2772.069 \text{ kg moles/day}$$

F of tower (2) is $(8.143 \times 3655.309)/100$

$$= 297.6510 \text{ Kg moles/day}$$

And D is $(5.1040 \times 3655.309)/100$

$$= 186.566 \text{ Kg moles/day}$$

And w is $(3.038 \times 3655.309)/100 = 111.048 \text{ Kg moles/day}$